

Full paper

Activate metallic copper as high-capacity cathode for lithium-ion batteries via nanocomposite technology



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ABSTRACT

In this work, metallic copper serving as a high-performance cathode in lithium-ion based carbonate electrolyte has been demonstrated. Computational modelling and in-situ ultraviolet-visible spectra confirm that Cu cathode experiences a two-electrons redox reaction: $\text{Cu} \leftrightarrow \text{Cu}^{2+} + 2\text{e}^-$ during charge/discharge process. By using one-dimensional (1D) nano-structure design and surface modification strategy, the Cu cathode delivers a reversible capacity of 635 mAh/g_{Cu} with a high output voltage of 3.61 V and affords a superior rate capability. With Li₄Ti₅O₁₂ as anode, a Cu/Li₄Ti₅O₁₂ full cell exhibits a discharge capacity of 601 mAh/g_{Cu} and an energy density of 1202 Wh/kg_{Cu}. The strategy of using metallic Cu as cathode in lithium-ion batteries is quite simple and broadly applicable, which may provide new opportunities for many other non-aqueous rechargeable batteries.

1. Introduction

Lithium-ion batteries (LIBs) are currently indispensable power supply for portable electronic devices due to their high energy density and good cyclability, which have generated great impacts on the human society [1]. To meet the ever-growing demand, increasing energy density and power density of LIBs has become research focus in battery community for decades [1–6]. The energy density of LIBs fundamentally depends on specific capacity of electrode materials and cell output voltage. Traditional electrode materials including layered metal oxides [7–11], polyanionic compounds [12–15], and layered graphite anodes [16–18] have limited space to accommodate enough Li ions, which deliver relatively low specific capacities due to the intercalation/deintercalation mechanism. On the other hand, the batteries based on conversion chemistry present much larger capacities, such as lithium-sulfur (Li-S) and lithium-oxygen (Li-O₂) batteries [19,20]. Since these systems meet many critical challenges especially poor cyclability, recent studies have shown that the batteries with conversion-type cathodes may be a good solution to reach 500 Wh/kg and offer comparable driving range for electric vehicles to conventional vehicles with internal

combustion engine [21,22].

Metallic copper (Cu) has evolved to fill many critical roles in industry and our daily life due to its abundance and high thermal/electrical conductivity. As we know, Cu can serve as a positive electrode in Daniell cell. The voltage of the cell is about 1.1 V in aqueous electrolyte by simply subtracting the potential of Zn²⁺/Zn redox couple (−0.76 V vs. SHE) from that of Cu²⁺/Cu redox couple (+0.34 V vs. SHE) [23]. In non-aqueous LIBs, Cu usually acts as current collector instead of electrode. In fact, the potential gap between Cu²⁺/Cu and Li⁺/Li is as high as 3.38 V according to the standard electrode potential table. Moreover, the theoretical capacity of Cu based on the two-electrons reaction ($\text{Cu} \leftrightarrow \text{Cu}^{2+} + 2\text{e}^-$) reaches 837 mAh/g [24]. Pairing Cu²⁺/Cu and Li⁺/Li electrodes theoretically gives an energy density as high as 2829 Wh/kg_{Cu}, which is almost comparable to Li-S batteries. This leads to a fundamental question: can metallic Cu directly serve as a cathode in non-aqueous battery systems to deliver a high voltage output?

The present challenge of coupling Cu/Li in a single organic electrolyte system lays on dissolution and diffusion of Cu²⁺ ions in electrolyte, which is similar to the well-known shuttle effect in Li-S batteries [25]. Many strategies have been proposed to solve the dissolution

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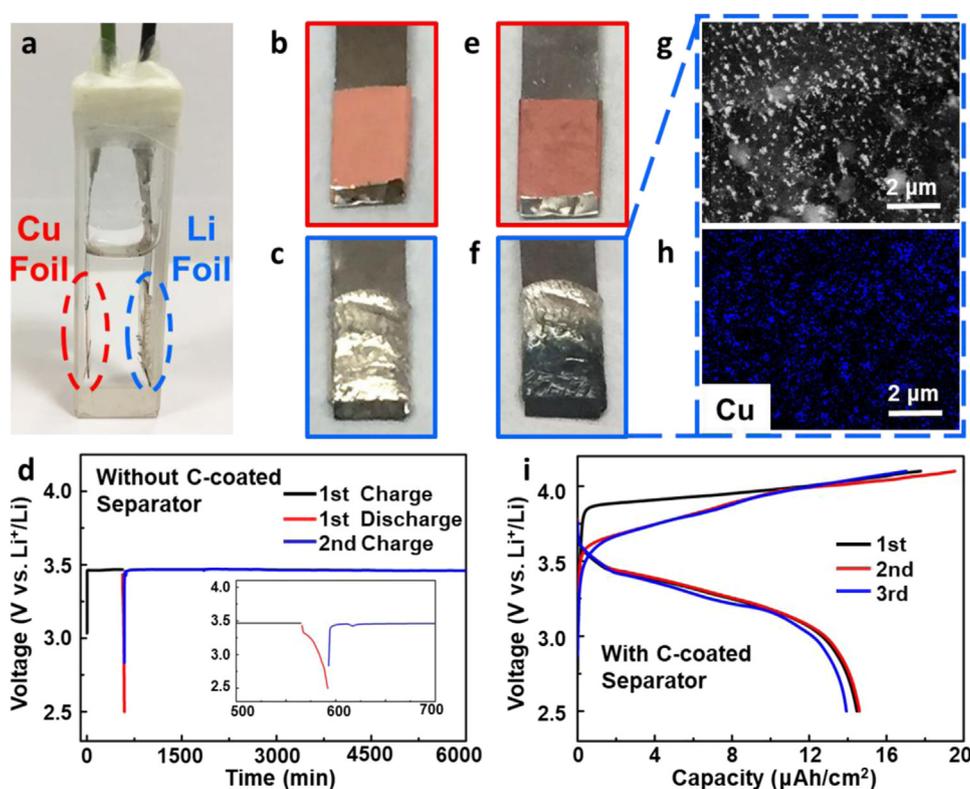


Fig. 1. (a) Optical photographs of the transparent half cell with (b) Cu foil cathode and (c) Li foil anode. (d) Galvanostatic charge/discharge curves of the transparent cell at a current of 0.05 mA g⁻¹. Optical photographs of (e) Cu foil cathode and (f) Li foil anode, (g, h) SEM and corresponding Cu elemental mapping images of Li foil anode after charging for 10 h. (i) Voltage profiles of coin-cell type Cu/Li half cell with a C-coated Celgard separator.

issue of polysulfides in Li-S batteries [26]. Inspired by the great progress of engineering separators in Li-S batteries [27], we demonstrate in this work that metallic Cu cathode can serve as a high-performance cathode in conventional non-aqueous LIBs. Theoretical calculation illustrated that the metallic Cu is oxidized to Cu²⁺ directly during charge process and the discharge process undergoes two steps: Cu²⁺ is first reduced to Cu⁺ and then further reduced back to metallic Cu. By using a nanosized metallic Cu/carbon nanofiber (Cu@CNFs) composite and a carbon-coated separator in the cell configuration [28,29], a high reversible capacity of 635 mAh/g_{Cu} with an average potential of 3.61 V (vs. Li⁺/Li) are obtained in a common carbonate electrolyte. To further improve the cycle stability, a simple surface modification strategy was employed, which enabled the Cu cathode exhibit a superior rate capability and along with a stable cycle performance. With Li₄Ti₅O₁₂ (LTO) as anode, the Cu/LTO full cell exhibits a high discharge capacity up to 601 mAh/g_{Cu}.

2. Results and discussion

The proof-of-concept study was demonstrated using a Cu/Li half cell within a home-made transparent device (Fig. 1a). Planar Cu foil (Fig. 1b and Fig. S1) acted as cathode, Li foil (Fig. 1c and Fig. S2) as anode and 1.0 M LiClO₄ in ethylene carbonate (EC)/propylene carbonate (PC) (v/v = 1/1) as electrolyte, while no separator was used. Galvanostatic charge started under 0.05 mA. As shown in Fig. 1d, the voltage of the cell increases rapidly and then a long voltage plateau appears at 3.45 V. This charge process corresponds to the oxidation of Cu foil along with dissolution of Cu²⁺ ions into electrolyte [30]. To keep the charge balance, Li⁺ ions in the electrolyte were reduced and deposited as metallic Li on Li foil. However, the charge process seems interminable over charging time. Thus, we manually stopped the charge process after 10 h and switched the current direction. Surprisingly, the cell presented an extremely short discharge process that the voltage sharply dropped to 2.5 V, suggestive of an irreversible process of Cu dissolution. This should be ascribed to that Cu²⁺ ions diffuse to the Li metal side and are then reduced by Li metal. To prove this hypothesis, we disassembled

the cell and characterized the Cu and Li foils after the charge process. The surface of Cu turned slightly grey and a great number of pits appeared (Fig. 1e and Fig. S3). On the anode side, Li foil became black (Fig. 1f). Scanning electron microscopy (SEM) and elemental mapping observation show that Li foil was covered by Cu-containing nanoclusters (Fig. 1g, h and Fig. S4). This indicates that Cu²⁺ ions diffused and deposited on Li foil by reacting with Li [31].

To suppress the diffusion of Cu²⁺ ions, we moved the electrodes into a coin cell and a C-coated Celgard polypropylene (PP) separator was employed (Fig. S5) [32]. As seen in Fig. 1i, the Cu/Li coin cell displays normal charge/discharge curves at a current of 0.05 mA. Compared to the transparent cell (Fig. 1d), the reversibility of Cu electrode in coin cell is greatly improved with the first-cycle coulombic efficiency reaching 75%. To verify the effect of C-coated separator, we examined the surface of Li foil after several cycles. The SEM and mapping images both show that there is no elemental Cu observed on the Li foil (Fig. S6). Overall, the above results prove that metallic Cu can be a reversible cathode for non-aqueous LIBs by simply adjusting the battery configuration. In the corresponding cyclic voltammetry (CV) curves (Fig. S7), a broad peak at 3.91 V appears during the initial anodic scan, indicating the oxidation of Cu while two peaks occurs at 3.52 and 3.33 V in the following cathodic scan present the reduction reactions: Cu²⁺ → Cu + and Cu + → Cu.

As shown in Fig. 1i, the specific capacity of the planar Cu foil is low due to the bulk morphology. To maximize the usage of metallic Cu, we designed a novel Cu@C composite cathode, in which active Cu nanoparticles were anchored on a three-dimensional conductive carbon nanofiber (CNFs) network. The detailed synthetic procedures are described in the Supporting information. The X-ray diffraction (XRD) pattern of Cu@CNFs demonstrate that metallic Cu is successfully obtained (Fig. 2a). SEM (Fig. 2b) and transmission electron microscope (TEM) images (Fig. 2c) show that Cu nanoparticles and CNFs have average sizes of 300 and 100 nm, respectively. A high-resolution TEM (HR-TEM) image (right side in Fig. 2c) on the edge of a single Cu nanoparticle displays a set of parallel fringes with d-spacing of 0.208 nm, corresponding to the (111) plane of Cu. Energy-dispersive X-ray

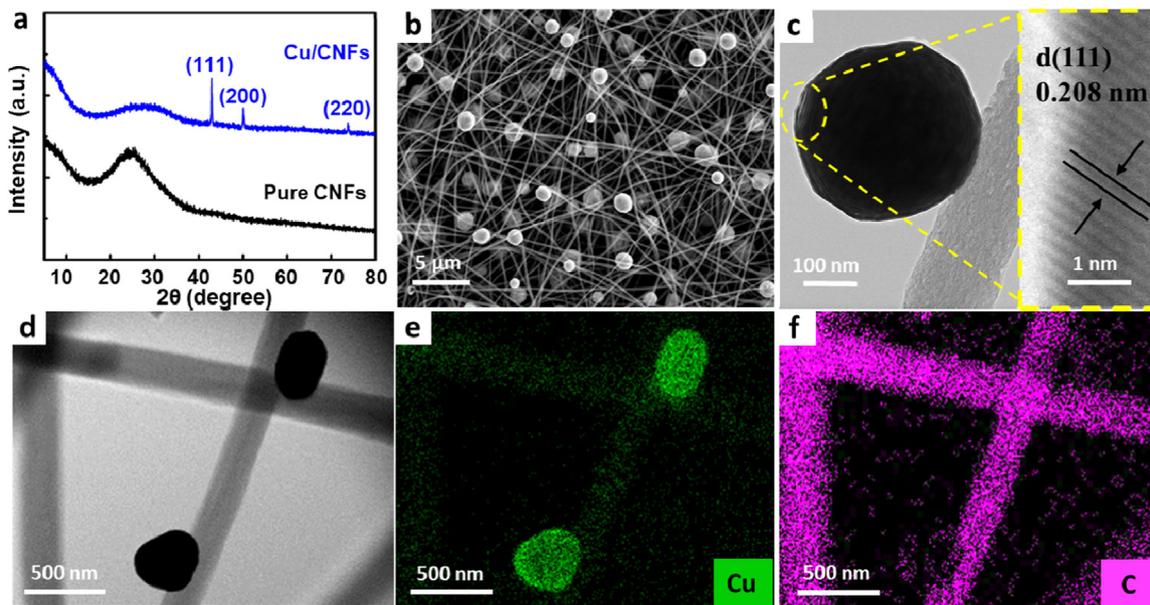


Fig. 2. Phase and morphology characteristics of Cu@CNFs composite. (a) XRD patterns of Cu/CNFs and pure CNF, (b) SEM, (c) TEM and (d-f) element mapping images of Cu@CNFs composite obtained by electrospinning and following thermal reduction.

spectroscopy (EDX) elemental mappings (Fig. 2d-f) show the distribution of Cu and C elements in the composite, demonstrating that Cu nanoparticles are well anchored on the CNFs.

The electrochemical performance of the Cu@CNFs composite was investigated by using the Cu@CNFs composite as cathode, Li foil as

anode and C-coated Celgard PP as separator. In Fig. 3a, the Cu@CNFs composite exhibits a relatively flat voltage plateau at 3.61 V. A specific capacity in charge as high as 770 mAh/g is attained, which reaches 91% of the theoretical capacity (837 mAh/g) based on two-electrons reaction. The corresponding discharge process exhibits a specific capacity of

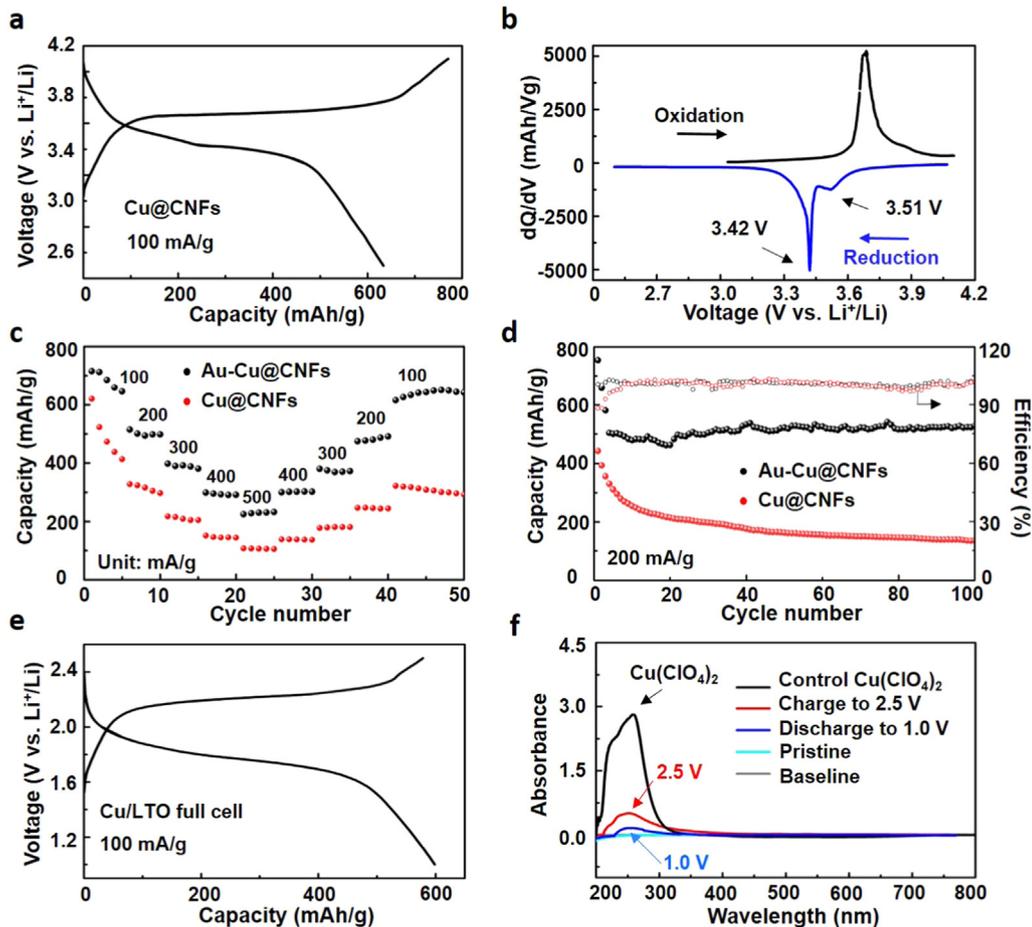


Fig. 3. (a) Voltage profile of Cu@CNFs electrode for the first cycle at 100 mA/g at room temperature. (b) The incremental charge versus potential (dQ/dV) curve of the charge/discharge process for Cu@CNFs electrode. (c) Specific discharge capacities of Cu@CNFs and Au-Cu@CNFs electrodes cycled at various current densities from 100 to 500 mA/g. (d) Cycling performance of Cu@CNFs and Au-Cu@CNFs electrodes at 200 mA/g. (e) Voltage profile of the full cell for the first cycle at 100 mA/g. (f) UV-vis absorption spectra of the electrolyte in the in-situ full cell at different states upon cycling.

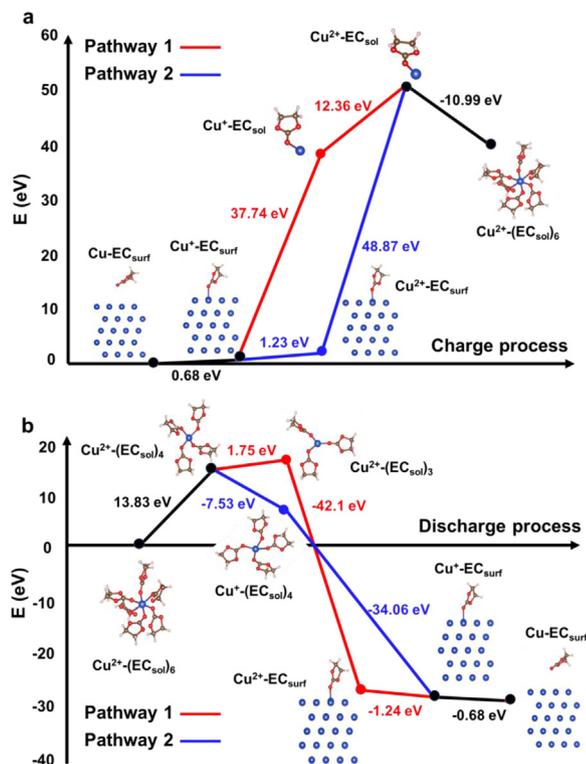


Fig. 4. Theoretical calculation for the redox process of Cu cathode in Cu/Li half cell. Two possible reaction pathways during (a) charge process and (b) discharge process, represented by red and blue lines, respectively. The blue line represents the energy-preferred pathway.

635 mAh/g, indicative of a highly reversible electrochemical redox reaction. Notably, the Cu@CNFs electrode exhibits one charge plateau corresponding to the oxidation process of $\text{Cu} \rightarrow \text{Cu}^{2+} + 2\text{e}^-$. In contrast, a weakly inflection point at 3.42 V divides the discharge curve into two parts. The two reduction steps are clearly evidenced by the incremental charge (dQ) versus potential (dQ/dV) curve (Fig. 3b) that the two cathodic peaks at 3.51 and 3.42 V should be ascribed to $\text{Cu}^{2+} \rightarrow \text{Cu}^+$ and $\text{Cu}^+ \rightarrow \text{Cu}$, respectively.

To understand the electrochemical process, the structure and morphology evolution of Cu@CNFs electrodes were monitored by ex-situ XRD and SEM measurements. In Fig. S8, the XRD peaks of metallic Cu nearly disappear after charging to 4.1 V. It is most likely that Cu was oxidized to Cu^{2+} and dissolved in the electrolyte. After discharge to 2.5 V, the Cu peak at 43° , 50° and 74° are completely restored, confirming that Cu^{2+} was reduced to Cu reversibly. The morphological change of Cu@CNFs composite agrees well with the structure evolution. As shown in Fig. S9, SEM images of Cu@CNFs after charging to 4.1 V display that there are no Cu nanoparticles anchored on the surface of CNFs. Inversely, metallic Cu is redeposited on the surface of CNFs after discharge to 2.5 V (Fig. S10). However, the re-deposited Cu aggregated and formed bulky particles, which is unfavorable to subsequent redox process. We speculate that the aggregation associates with the low surface energy and affinity of Cu^{2+} on CNFs surface [33].

To prevent the aggregation of Cu on CNFs upon repeated cycles, a simple Au nanoparticle coating was applied [34]. SEM images of Au-coated Cu@CNFs (Au-Cu@CNFs) show that Au nanoparticles with diameter from 5 to 20 nm are uniformly covered onto the Cu/CNFs surface (Fig. S11). Interestingly, Au-Cu@CNFs composite exhibits charge capacity of 755 mAh/g and discharge capacity of 751 mAh/g in the first cycle (Fig. S12), indicating an initial coulombic efficiency (CE) as high as 99%. Furthermore, the rate capability of Au-Cu@CNFs is also enhanced compared to Cu@CNFs electrode. As seen in Fig. 3c, the reversible discharge specific capacities of Au-Cu@CNFs are 720, 541,

398, 299 and 225 mAh/g at current densities of 100, 200, 300, 400 and 500 mA/g, respectively. The capacity can be recovered up to 615 mAh/g when the current density turns back to 100 mA/g, suggesting an excellent rate capability. Moreover, Au-Cu@CNFs displays superior long-term stability with a specific capacity of 523 mAh/g at 200 mA/g over 100 cycles (Fig. 3d). To verify the role of Au modification, the morphology of Au-Cu@CNFs composite during redox process were investigated by SEM (Fig. S13) and TEM (Fig. S14). The morphology of Au-Cu@CNFs shows that Cu nanoparticles disappear while Au nanoparticles still adheres on the surface of CNFs after charging to 4.1 V and the redeposited Cu nanoparticles have no aggregation. The morphology change validates that Au modification provides more nucleation sites, and hence promotes the uniform deposition of Cu.

A full cell composed of Au-Cu@CNFs composite cathode and $\text{Li}_4\text{Ti}_5\text{O}_{12}$ (LTO) anode was further fabricated. The charge process of the full cell corresponds to the oxidation from Cu to Cu^{2+} in cathode side and the intercalation of Li ions into LTO in anode side (Fig. S15). The SEM images (Fig. S16) and charge/discharge curve (Fig. S17) of LTO anode are given in the Supporting information. The full cell displays an average working voltage of 2.0 V and delivers a discharge specific capacity of 601 mAh/g (Fig. 3e). To investigate the redox mechanism of metallic Cu in full cell, an in-situ transparent cell using Cu@CNFs cathode and LTO anode was assembled and the electrolyte was tested by UV-vis radiation upon electrochemical reactions. Compared to pristine electrolyte, a new peak located at 257 nm appears after charging to 2.5 V. The new peak corresponds to the characteristic peak of $\text{Cu}(\text{ClO}_4)_2$ (Fig. 3f), which proves the formation of $\text{Cu}(\text{ClO}_4)_2$ by: $\text{Cu} + 2\text{LiClO}_4 \rightarrow \text{Cu}(\text{ClO}_4)_2 + 2\text{Li}^+$. After discharging to 1.0 V, the $\text{Cu}(\text{ClO}_4)_2$ peak almost disappears, suggesting that most of Cu^{2+} ions are reversibly reduced while a small amount of Cu^{2+} ions are maintained in the electrolyte. This result further demonstrates the electrochemical process we proposed in Cu/Li half cells.

To further understand the electrochemical process of non-aqueous Cu/Li cell, we employed computational modelling based on density functional theory (DFT). The detailed calculation procedure is described in Supporting information. For the charge process, the theoretical calculation confirms that Cu atoms can uptake one solvent molecule and form Cu-solvent at Cu (111) surface before oxidation. The as-formed $\text{Cu-EC}_{\text{surface}}$ ($\text{Cu-EC}_{\text{surf}}$) is continuously oxidized with EC absorption, and finally formed $\text{Cu}^{2+}-(\text{EC}_{\text{sol}})_6$ since $\text{Cu}^{2+}-(\text{EC}_{\text{sol}})_6$ is the most stable structure (Fig. S18). For the charge process, there are two possible pathways (Fig. 4a): one is that $\text{Cu-EC}_{\text{surf}}$ is oxidized to $\text{Cu}^+-\text{EC}_{\text{surf}}$ at Cu (111) surface and diffuses to the electrode/electrolyte interface to complete oxidation and absorption; the other is that $\text{Cu-EC}_{\text{surf}}$ is directly oxidized to $\text{Cu}^{2+}-\text{EC}_{\text{surf}}$ at Cu (111) surface and then forms $\text{Cu}^{2+}-(\text{EC}_{\text{sol}})_6$ by absorbing more EC molecules. The corresponding energy values are illustrated in Fig. 4a, and the energies of $\text{Cu-EC}_{\text{surf}}$, $\text{Cu}^+-\text{EC}_{\text{surf}}$ and $\text{Cu}^{2+}-\text{EC}_{\text{surf}}$ are listed in Table S1. The reaction energy for $\text{Cu}^+-\text{EC}_{\text{surf}} \rightarrow \text{Cu}^+-\text{EC}_{\text{sol}}$ (pathway 1) is 37.74 eV while that for $\text{Cu}^+-\text{EC}_{\text{surf}} \rightarrow \text{Cu}^{2+}-\text{EC}_{\text{surf}}$ (pathway 2) is only 1.23 eV. Obviously, the latter pathway is more favorable. Therefore, we believe that Cu is directly oxidized to Cu^{2+} at Cu (111) surface. Similarly, the following reduction reaction in the discharge process has also two possible pathways, as shown in Fig. 4b. According to the calculation, the reaction energy for $\text{Cu}^{2+}-(\text{EC}_{\text{sol}})_4 \rightarrow \text{Cu}^{2+}-(\text{EC}_{\text{sol}})_3$ (1.75 eV) pathway 1 is much higher than that of $\text{Cu}^{2+}-(\text{EC}_{\text{sol}})_4 \rightarrow \text{Cu}^+-\text{EC}_{\text{sol}}$ (-7.53 eV) pathway 2. Thus, the pathway 2 is preferred. We further calculated the average voltage of Cu redox process in Cu/Li half cell on the basis of the above-discussed pathways. The calculated average voltage is 3.83 V, which is close to the experimental value. Both the experimental measurement and theoretical calculation demonstrate that Cu cathode experiences a two-electrons redox reaction ($\text{Cu} \leftrightarrow \text{Cu}^{2+} + 2\text{e}^-$) during charge/discharge processes.

3. Conclusion

In summary, we have demonstrated metallic copper as a splendid cathode material for non-aqueous LIBs through a two-electrons conversion reaction. The as-designed Cu@CNFs nanocomposite exhibits a high output voltage of 3.61 V in LIBs system and delivers a high energy density of 2292 Wh/kg_{Cu}. A simple surface modification by Au coating facilitates the nucleation and growth of Cu upon discharge, which hinders the aggregation of Cu particles and improves the rate and cycling capabilities of Cu cathode. We anticipate that the Cu cathode with high output voltage, high capacity and good stability in non-aqueous LIB systems is available for developing next-generation batteries to meet the ever-growing demand of high energy density. Furthermore, since the reversible redox reaction of Cu cathode is independence of the metal ions in electrolyte salt, we believe that Cu cathode can be further extended to other metal-ion battery systems.

4. Experimental section

4.1. Fabrication of the transparent half cell and full cell

The transparent half cell and in-situ full cell were assembled in cuvettes (size: 12.5(W)*12.5(L)*45(H) mm). For the transparent half cell, Cu foil and Li foil were fixed on two titanium (Ti) foils respectively (size: 6(W)*60(L) mm) using as cathode and anode. Cu@CNFs composite was fixed on a Ti foil as cathode and Li₄Ti₅O₁₂ slurry was casted onto a Ti foil as anode for the in-situ full cell. 1.0 mol/L LiClO₄ EC/PC (v/v = 1:1) electrolyte was used in two cases.

4.2. Synthesis of electrodes and C-coated separators

4.2.1. Cu@CNFs composite

The Cu@CNFs composite was synthesized by electrospinning and subsequent thermal reduction. The electrospinning precursor solution was made by blending 1 g polyacrylonitrile (PAN) and 0.5 g copper acetate monohydrate (Cu(CH₃COO)₂·H₂O) in 10 mL N, N-Dimethylformamide (DMF). The precursor solution was kept at 80 °C and stirred for 12 h. Then a high-voltage of 17 kV was applied to the solution during the electrospinning process. The collected fibers were stabilized at 280 °C for 3 h in air and further carbonized at 900 °C for 2 h in H₂/Ar (5% H₂) atmosphere, the heating rate for stabilization and carbonization are 5 °C/min. The final product Cu@CNFs composite film was cut into disks with 8 mm diameter and used as electrode directly. Thermogravimetric analysis (TGA) gives the Cu content in Cu@CNF composite, which is about 50 wt% (Fig. S19). The loading for each electrode is 0.5 mg/cm².

4.2.2. Au-Cu@CNFs composite

The Au nanoparticles were directly deposited on the Cu@CNFs surface by Precision etching coating instrument (Gatan 682). The coating time is 150 s and the particles size of Au are 5–20 nm.

4.2.3. Li₄Ti₅O₁₂ electrode

The Li₄Ti₅O₁₂ electrode is consisted of 60 wt% Li₄Ti₅O₁₂, 30 wt% Super P and 10 wt% PVDF. All components were mixed and ground with N-methyl-2-pyrrolidinone solvent to prepare the slurry, casted onto a Cu current collector and completely dried before use. The Loading of LTO is about 2 mg/cm².

4.2.4. C-coated separator

The C-coated separator is prepared by uniformly casting carbon slurry on Celgard 2301 polypropylene separator and dried before use. The carbon slurry is consisted of 60 wt% Super P, 20 wt% active carbon and 20 wt% PVDF. All components were mixed and ground with N-methyl-2-pyrrolidinone (NMP) solvent to prepare the slurry.

4.3. Material characterizations

The material morphology was investigated by SEM (SIRION200) and TEM (FEI Tecnai G2 F30). Structure of materials were detected by XRD (PANalytical X'pert PRO-DY2198, Holland) measurements. TG (NETZSCH STA449F3) analysis was carried out in air from room-temperature to 800 °C at a heating rate of 10 °C/min. In-situ UV–vis spectrum was detected on a UV-2550 UV–vis spectrophotometer (Shimadzu, Japan).

4.4. Electrochemical measurements

All the cells were assembled in an argon-filled glove box (O₂ and H₂O less than 1 ppm). In coin-cells, the cathode and anode were separated by a carbon coated Celgard separator. 1.0 M LiClO₄ dissolved in a mixture of ethylene carbon (EC) and propylene carbonate (PC) (1:1 by volume) was used as the electrolyte for LIBs. Galvanostatic charge-discharge tests were carried out on a Neware Battery Measurement System at various current densities. CV measurements in the voltage range of 2.5–4.1 V vs. Li⁺/Li with a scanning rate of 0.05 mV/s were carried out on a CHI 760E electrochemical workstation.

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Appendix A. Supporting information

Supplementary data associated with this article can be found in the online version at [doi:10.1016/j.nanoen.2018.09.064](https://doi.org/10.1016/j.nanoen.2018.09.064)

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